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# ARE THE LESSONS OF THE TECHNO-ECONOMIC STUDIES ON THE SULPHUR-IODINE CYCLE APPLICABLE TO THE OTHER CYCLES?

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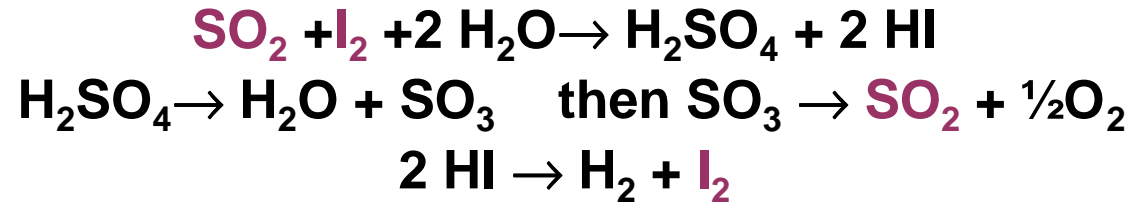
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- On the potentiality of the Sulphur-Iodine (S-I) cycle
- Alternative thermochemical cycles and compatibilities with Generation IV nuclear reactors
- Recommendations for guiding the selection of alternative cycles

# On the potentiality of the S-I cycle



- The temperature at which  $\text{O}_2$  is created is high ( $T \geq 850^\circ\text{C}$ ) → the energy efficiency  $\eta_T$  could be high.
- In the case where the work (W) and the heat (Q) necessary for the process are produced from a Very High Temperature Reactor

$$\eta_T = \text{HHV} / [Q + (W / \eta_{el})]$$

Where the electricity is produced with an energy efficiency  $\eta_{el}$

And HHV is the high heating value of hydrogen

# Limits for the competitiveness of the S-I Cycle (1)



It is necessary at first, to compare with a reference chain:

*I-tésé* Heat from the reactor → electricity → hydrogen from alkaline electrolysis.

$\eta_T$  the net efficiency the S-I cycle will have to be higher than that of the reference chain defined by:

$$\eta_{Ref} = \eta_{el} \times \eta_{electrolyzer}$$

- Where  $\eta_{electrolyzer}$  is the efficiency of the transformation electricity → hydrogen
- NorskHydro company has developed devices with  $\eta_{electrolyzer} = 73 \%$
- it is generally assumed that for a VHTR  $\eta_{el} \approx 47 \% \Rightarrow \eta_{Ref} = 34 \%$ .

*Due to the complexity of the S-I cycle, the investment and maintenance costs would be higher than those of the reference chain*

**A first limit to the competitiveness :  $\eta_T > \eta_{Ref} = 34 \%$ .**

## Limits for the competitiveness of the S-I Cycle (2)

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- Different studies, from France and USA *which assess the long term evolution of the Steam Methane Reforming , as well as the progressive implementation of 3<sup>rd</sup> Generation nuclear reactors coupled with large alkaline electrolysis plants*
- estimated that in the future, the new processes for producing hydrogen should reach

**a target between 2 to 3 \$/kg of H<sub>2</sub> .**

- This provided a second limit for the competitiveness of the S-I cycle coupled with a HTR

# On the present knowledge of the S-I cycle



- Chemical reactions are usually not complete; as a matter of fact, the consumption of energy needed for the decomposition of HI is higher than expected.
- Excess of H<sub>2</sub>O and I<sub>2</sub> at the outlet of the Bunsen reactor are needed to avoid miscibility of HI and H<sub>2</sub>SO<sub>4</sub> acids. These lead to high material circulation and heat needs.
- Heat management will be optimised in order to reach a correct balance between the recovery of the heat and the size of the apparatus.

**Generic improvements of the basic operations are currently studied by CEA**

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# Alternative thermochemical cycles and compatibilities with Generation IV nuclear reactors

- **The Generation IV International forum (GIF) has retained six innovative concepts of nuclear reactors.**
- **M.A Lewis (Argonne) selected four promising alternative pure thermochemical cycles.**

# Innovative concepts of nuclear reactors

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I-tésé

1. the Gas Fast Reactor (GFR)  $T_{oc} \in [550-850^{\circ}\text{C}]$ ,
2. the Molten Salt Reactor (MSR)  $T_{oc} \in [640-850^{\circ}\text{C}]$ ,
3. the Lead Fast Reactor (PbFR)  $T_{oc} \in [520-620^{\circ}\text{C}]$ ,
4. the Sodium Fast Reactor (SFR)  $T_{oc} \in [500-640^{\circ}\text{C}]$ ,
5. the Supercritical Water Reactor (SCWR)  $T_{oc} \in [380-500^{\circ}\text{C}]$ ,
6. the Very High Temperature Reactor (VHTR)  $T_{oc} \in [880-1000^{\circ}\text{C}]$ .

$T_{oc}$  is the temperature at the outlet of the reactor core

## Promising alternative thermochemical cycles

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- I. Cerium-Chlorine (Ce-Cl)  $T_h = 850^\circ\text{C}$ ,
- II. Magnesium-Iodine (Mg-I)  $T_h = 600^\circ\text{C}$ ,
- III. Iron-Chlorine (Fe-Cl)  $T_h = 739^\circ\text{C}$ ,
- IV. Vanadium-Chlorine (V-Cl)  $T_h = 770^\circ\text{C}$ .

$T_h$  is the temperature of the hotter point for each cycle:  
i.e. the temperature at which  $\text{O}_2$  is produced

## Compatibility between reactors and cycles (1)



	<b>Ce-Cl</b>	<b>Mg-I</b>	<b>Fe-Cl</b>	<b>V-Cl</b>
<b>GFR</b>	No	Yes [+]	Yes [+]	Yes [+]
<b>MSR</b>	No	Yes [- +]	Yes [+]	Yes [+]
<b>PbFR</b>	No	No	No	No
<b>SFR</b>	No	Yes [+]	No	No
<b>SCWR</b>	No	No	No	No
<b>VHTR</b>	Yes [+]	Yes [- +]	Yes [- +]	Yes [- +]

+ corresponds to the upper bound among the studied values for the outlet core temperature,  
- to the lower bound.

## Compatibility between reactors and cycles (2)

It appears that, at the present stage of knowledge:

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*I-tésé*

- all the four alternative cycles selected, would be compatible with the VHTR,
- none of them with the PbFR and the SCWR.
- the Magnesium-iodine (Mg-I) is compatible with the SFR, the GFR and the MSR,
- the chlorine based cycles: Iron-Chlorine (Fe-Cl) and Vanadium-Chlorine (V-Cl) are both compatible with the GFR and MSR,

# The alternative cycle and the first limit of competitiveness

— considering a NorskHydro alkaline electrolyser with  $\eta_{el} = 73\%$ ,  
And the efficiencies  $\eta_{el}$  for producing electricity from the reactors



$$\eta_{Ref} = \eta_{el} \times \eta_{electrolyzer}$$

- **it is possible to define values of the net efficiency ( $\eta_T$ ) that an alternative cycle coupled with a given reactor will have to exceed**

*Due to the complexity of all the thermochemical cycles, they would lead to investment and maintenance costs higher than those of the reference chain of the selected reactor*

	$\eta_{el}$ [%]	$\eta_T$ [%]
<b>GFR</b>	<b>42</b>	<b>&gt; 31</b>
<b>MSR</b>	<b>29</b>	<b>&gt; 21</b>
<b>PbFR</b>	<b>44</b>	<b>&gt; 32</b>
<b>SFR</b>	<b>40</b>	<b>&gt; 29</b>
<b>VHTR</b>	<b>47</b>	<b>&gt; 34</b>

## The alternative cycle and the second limit of competitiveness

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*Somewhat more complex to express than the first limit.*



- **The energy consumption must be very carefully estimated, particularly for the reactions which produce H<sub>2</sub>. These reactions are not spontaneous. Heat management will be optimised in order to reach a correct balance between the recovery of the heat and the size of the apparatus.**
- **The cost of electricity must be precisely assessed. For Generation IV reactors, the cost of electricity and the total failure probability could be greater than for Generation III reactors.**
- **The cost of the coupling between the reactor and the thermochemical cycle must be investigated in terms of investment, additional energy consumption and safety consideration.**

# Conclusions

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- Among the promising thermochemical cycles studied with a view to produce hydrogen from nuclear reactors, and given the present state of knowledge, most of them would only be compatible with VHTRs.

**The future of these cycles should strongly depend on the VHTRs.**

***And conversely the future of the VHTRs will depend on their interest for producing hydrogen***

- In any cases, the sets reactor + thermochemical cycles will be confronted with limits of competitiveness.
- Critical points have been identified, which are currently examined by CEA.

**CEA will realize a deeper assessment of the thermochemical cycles at the end of 2008.**