



**ICENES 2007**  
03 - 08 June 2007  
Istanbul - Turkey

# Multiphysics Methods Development for High Temperature Gas Cooled Reactor Analysis

V. Seker (PU)  
T. Downar (UCB)

June 8<sup>th</sup>, 2007

# Outline

---

- Motivation
- Thermal Hydraulics Model
- Neutronics Model
- Cross Section models and coupling
- Verification studies;
  - Simulation of SANA experiment
  - PBMR-400 Benchmark problem
- Summary and Future Work

# Motivation

---

- To develop multiphysics methods in a **system analysis** code for;
  - calculating the **thermal-hydraulics** and **neutronics** parameters
  - predicting the transient behavior of the reactor **accurately** and **efficiently** under any anticipated accident conditions.

# Specific Research Objectives

---

- Development of a thermal-hydraulics computer code to calculate the **temperature and flow field**:
  - Use the porous media approach with pebble bed effective conductivity, resistance coefficient, and solid-to-fluid heat transfer coefficient (experimental data)
  - 3-D, Cylindrical coordinates
  - Steady-state, transient conditions

# Cont ... (Specific Research Objectives )

---

- Modification of the existing 3-D cylindrical neutronics solver in PARCS code
  - implementation of new features
    - Anisotropic diffusion coefficients
    - Periodic boundary conditions for the azimuthal direction
  - Adjustments to perform the calculations of steady-state conditions for all anticipated transient scenarios

# Cont ... (Specific Research Objectives )

---

- Development of methods to perform an efficient and accurate coupling of the thermal-hydraulics and neutronics solutions.
- Verification of methods by simulating Pebble Bed experiments and benchmark problems.

# T/H Codes for PBMR

---

- **THERMIX-KONVEK & THERMIX-DIREKT**
- THERMIX
  - Temperature calculation
  - Two-temperature porous media model
  - Steady-State and time dependent
  - 2-D (r-z) cylindrical coordinates

# Cont ... (Current Codes)

---

- KONVEK
  - Flow field calculation
  - Porous media approach
  - **Steady-state (quasi-static)**
  - 2-D (r-z) cylindrical coordinates
- DIREKT
  - Flow field calculation
  - Porous media approach
  - **S.S. and time dependent**
  - 2-D (r-z) cylindrical coordinates

# Developed Methods

---

- PARCS/THERMIX-3D
  - Thermal/hydraulics Solver
    - 3-D cylindrical coordinates, porous media, time dependent & steady state
  - Neutronics
    - 3-D cylindrical coordinates, finite difference, neutron diffusion

# Thermal Hydraulics Model

---

## Mass Balance

$$\frac{\partial}{\partial t}(\epsilon \rho_f) + \nabla \cdot (\rho_f \mathbf{v}_f) = 0$$

## Momentum Balance

$$\frac{\partial(\rho \vec{v})}{\partial t} + \nabla \cdot (\rho \vec{v} \cdot \vec{v}) = -\nabla p + \nabla \cdot \bar{\tau} + \rho \vec{g}$$

## Energy Balance

Two-Temperature Model (next slide)

# Two-Temperature model

---

Solid Medium

$$\frac{\partial}{\partial t} \left[ (1 - \varepsilon) \rho_s c_{p_s} T_s \right] = \nabla \cdot (1 - \varepsilon) k_s \nabla T_s - \alpha (T_s - T_f) + Q$$

Fluid Medium

$$\frac{\partial}{\partial t} \left[ \varepsilon \rho_f c_{p_f} T_f \right] + \nabla \cdot (\rho_f c_{p_f} u T_f) = \nabla \cdot \varepsilon k_f \nabla T_f - \alpha (T_f - T_s)$$

# Neutronics Model

---

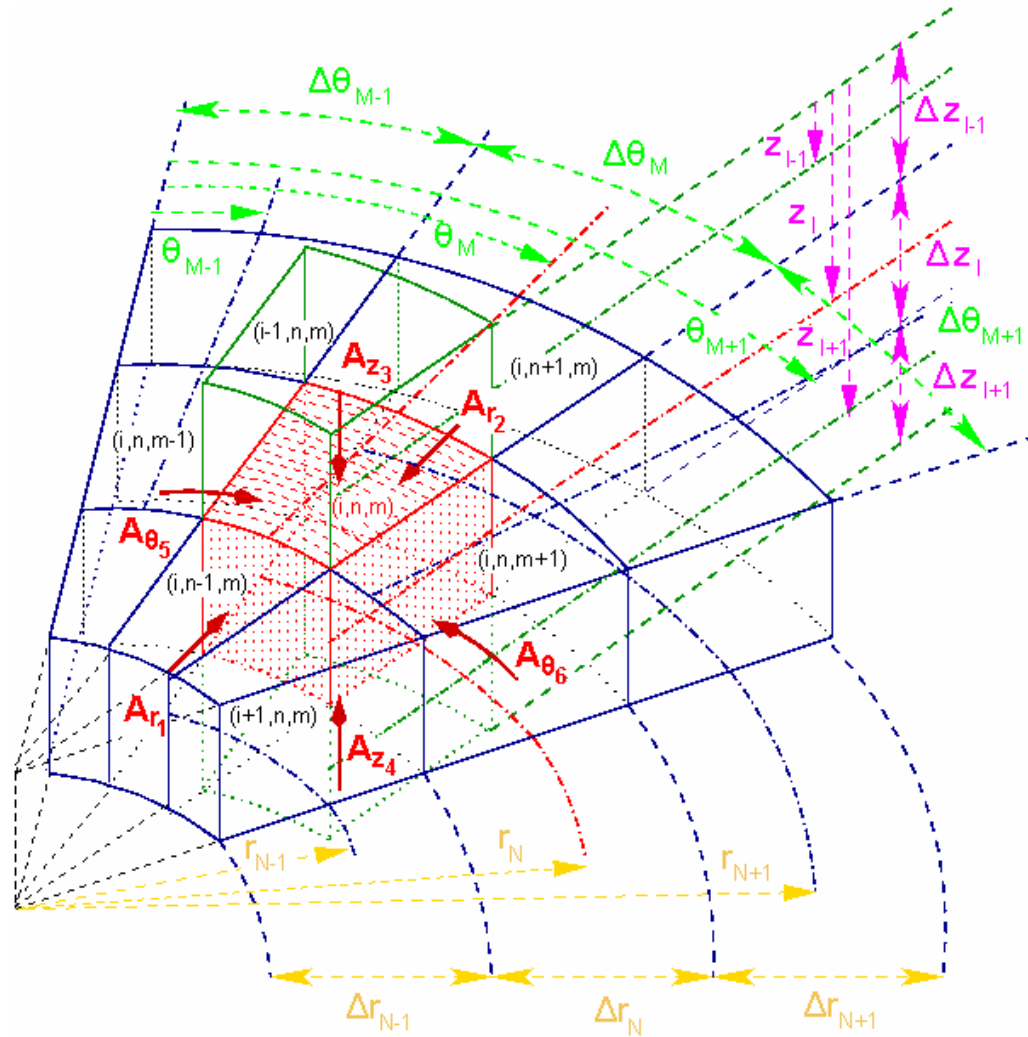
## Neutron Balance Equation

$$\frac{1}{v_g} \frac{d\phi_g}{dt} = \frac{\chi_{pg}}{k_{eff}} \sum_{g=1}^G v_{pg} \Sigma_{fg} \phi_g + \chi_{dg} \sum_{k=1}^K \lambda_k C_k + \sum_{g'=1(g' \neq g)}^G \Sigma_{sg'g} \phi_{g'} - \Sigma_{tg} \phi_g + \nabla \cdot D_g \nabla \phi_g$$

## Precursor Concentration

$$\frac{dC_k}{dt} = \frac{1}{k_{eff}} \sum_{g=1}^G v_{dgk} \Sigma_{fg} \phi_g - \lambda_k C_k$$

# Control Volume



# Discretization Equation

---

- Spatial discretization
  - Finite volume
  - General Scheme for convective terms including, CD, UDS, Hybrid, Power Law and Exponential
- Temporal discretization
  - Theta method
    - 0 = fully explicit
    - 1 = fully implicit
    - 0.5 = Crank-Nicholson

# Discretization of the Energy Balance Equation

---

- Solid Energy Equation in Cylindrical Coordinates

$$\begin{aligned} \frac{\partial}{\partial t} \left[ (1 - \varepsilon) \rho_s c_{p_s} T_s \right] &= \frac{1}{r} \frac{\partial}{\partial r} \left( (1 - \varepsilon) k_s r \frac{\partial T_s}{\partial r} \right) + \frac{1}{r} \frac{\partial}{\partial \theta} \left( (1 - \varepsilon) \frac{k_s}{r} \frac{\partial T_s}{\partial \theta} \right) \\ &+ \frac{\partial}{\partial z} \left( (1 - \varepsilon) k_s \frac{\partial T_s}{\partial z} \right) - \alpha (T_s - T_f) + Q \end{aligned}$$

# Final Form of The Solid Energy Equation

---

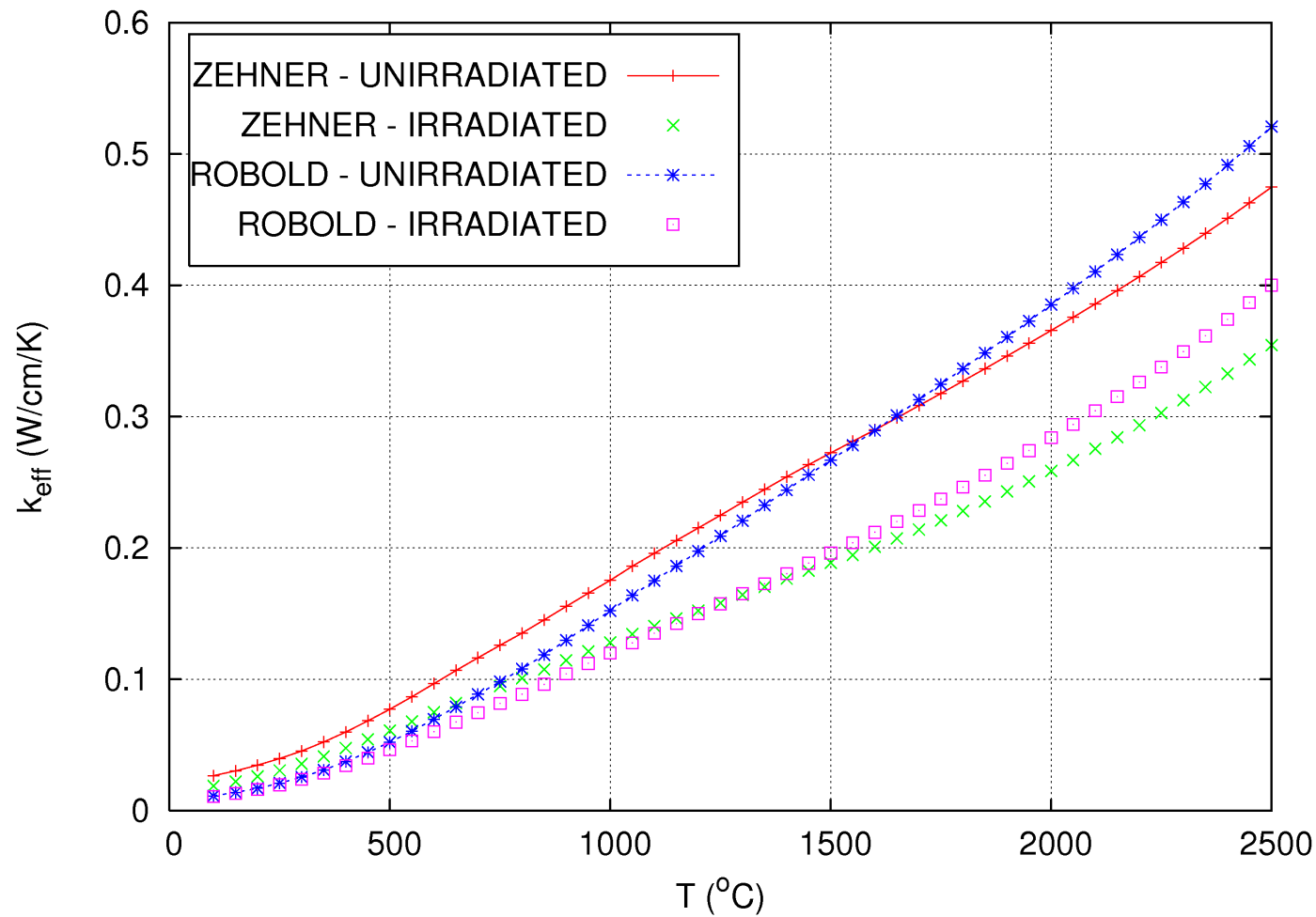
$$\begin{aligned}
 & \left[ (1-\varepsilon)_P (\rho c_p)_{s,P} \frac{\Delta V}{\Delta t} + \Theta (D_e + D_w + D_n + D_s + D_t + D_b + \alpha \Delta V) \right] T_{s,P} \\
 - & \Theta D_e T_{s,E} - \Theta D_w T_{s,W} - \Theta D_n T_{s,N} - \Theta D_s T_{s,S} - \Theta D_t T_{s,T} - \Theta D_b T_{s,B} \\
 = & (1-\varepsilon)_P^o (\rho c_p)_{s,P}^o \frac{\Delta V}{\Delta t} T_{s,P}^o + \Theta \Delta V (\alpha T_{f,P} + Q) \\
 + & \left[ D_e^o T_{s,E}^o + D_w^o T_{s,W}^o + D_n^o T_{s,N}^o + D_s^o T_{s,S}^o + D_t^o T_{s,T}^o + D_b^o T_{s,B}^o \right. \\
 & \quad \left. - (D_e^o + D_w^o + D_n^o + D_s^o + D_t^o + D_b^o) T_{s,P}^o \right. \\
 & \quad \left. - \alpha^o (T_{s,P}^o - T_{f,P}^o) \Delta V + Q \Delta V \right] (1-\Theta)
 \end{aligned}$$

Variable Porosity and Effective Thermal Conductivity

$$\varepsilon = f(r, \theta, z)$$

$$k = f(T, D) \quad D: \text{Fast Neutron Dose}$$

# Effective Thermal Conductivity of Pebble Bed



# Fluid Energy Equation in Cylindrical Coordinates

---

$$\begin{aligned} \frac{\partial}{\partial t} \left[ (\varepsilon \rho_f c_{p_f} T_f) \right] &= -\frac{1}{r} \frac{\partial}{\partial r} \left( r \rho_f c_{p_f} u_r T_f \right) - \frac{1}{r} \frac{\partial}{\partial \theta} \left( \rho_f c_{p_f} u_\theta T_f \right) - \frac{\partial}{\partial z} \left( \rho_f c_{p_f} u_z T_f \right) \\ &+ \frac{1}{r} \frac{\partial}{\partial r} \left( \varepsilon k_f r \frac{\partial T_f}{\partial r} \right) + \frac{1}{r} \frac{\partial}{\partial \theta} \left( \varepsilon \frac{k_f}{r} \frac{\partial T_f}{\partial \theta} \right) \\ &+ \frac{\partial}{\partial z} \left( (1 - \varepsilon) k_s \frac{\partial T_s}{\partial z} \right) - \alpha (T_f - T_s) \end{aligned}$$

# Final Form of The Gas Energy Equation

---

$$\begin{aligned}
 & \left[ \varepsilon_P (\rho c_p)_{f,P} \frac{\Delta V}{\Delta t} + \Theta (A_E + A_W + A_N + A_S + A_T + A_B + \alpha \Delta V) \right] T_{f,P} \\
 - & \Theta (A_E T_{f,E} + A_W T_{f,W} + A_N T_{f,N} + A_S T_{s,S} + A_T T_{f,T} + A_B T_{f,B}) \\
 = & \varepsilon_P^o (\rho c_p)_{f,P}^o \frac{\Delta V}{\Delta t} T_{f,P}^o + \Theta \Delta V \alpha T_{s,P} \\
 + & \left[ A_E^o T_{f,E}^o + A_W^o T_{f,W}^o + A_N^o T_{f,N}^o + A_S^o T_{f,S}^o + A_T^o T_{f,T}^o + A_B^o T_{f,B}^o \right. \\
 & \quad - (A_E^o + A_W^o + A_N^o + A_S^o + A_T^o + A_B^o) T_{f,P}^o \\
 & \quad \left. - \alpha^o (T_{f,P}^o - T_{s,P}^o) \Delta V \right] (1 - \Theta)
 \end{aligned}$$

# Coefficients

$$A_E = D_e A(|P_e|) + \llbracket -F_e, 0 \rrbracket$$

$$A_W = D_w A(|P_w|) + \llbracket F_w, 0 \rrbracket$$

$$A_S = D_s A(|P_s|) + \llbracket -F_s, 0 \rrbracket$$

$$A_N = D_n A(|P_n|) + \llbracket F_n, 0 \rrbracket$$

$$A_T = D_t A(|P_t|) + \llbracket -F_t, 0 \rrbracket$$

$$A_B = D_b A(|P_b|) + \llbracket F_b, 0 \rrbracket$$

Scheme	Expression for A( P )
Central difference	$1 - 0.5 P $
Upwind	1
Hybrid	$\llbracket 0, 1 - 0.5 P  \rrbracket$
Power Law	$\llbracket 0, (1 - 0.5 P )^{0.5} \rrbracket$
Exponential	$ P  / [\exp( P ) - 1]$

$$P = \frac{D}{F} \quad : \text{Peclet Number}$$

# Flow Field Calculation

---

- The resistance term is introduced into the momentum equation using a simplification in the momentum equation. (applied in TINTE, THERMIX-KONVEK and THERMIX-DIREKT)

$$\frac{\partial(\rho\vec{v})}{\partial t} + \nabla \cdot (\rho\vec{v} \cdot \vec{v}) = -\nabla p + \nabla \cdot \bar{\tau} + \rho\vec{g}$$

$$\nabla \cdot (\rho\vec{v} \cdot \vec{v}) - \nabla \cdot \bar{\tau} = W \cdot \rho\vec{v}$$

# Simplified Momentum Equation

---

$$\frac{\partial(\rho\vec{v})}{\partial t} = -W \cdot \rho\vec{v} - \nabla p + \rho\vec{g}$$

$$W = \zeta \frac{(1-\varepsilon)}{\varepsilon^3} \frac{1}{d_p} \frac{|\rho v|}{2\rho}$$

$\varepsilon$  = porosity

$d_p$  = particle diameter

$\zeta$  = resistance cofactor (experimentally determined)

$$\zeta = \frac{320}{(\text{Re}/(1-\varepsilon))} + \frac{6}{(\text{Re}/(1-\varepsilon))^{0.1}} \quad (\text{for pebble bed})$$

# Discretization of the Momentum Equation

---

$$\frac{\partial(\rho\vec{v})}{\partial t} = \frac{1}{A} \frac{\partial \dot{m}}{\partial t}$$

$$\frac{1}{A_{r1}} \frac{d\dot{m}_1}{dt} = -\frac{W_1}{A_{r1}} \dot{m}_1 - \frac{\Delta p_1}{(r_N - r_{N-1})}$$

$$\frac{1}{A_{r2}} \frac{d\dot{m}_2}{dt} = -\frac{W_2}{A_{r2}} \dot{m}_2 - \frac{\Delta p_2}{(r_{N+1} - r_N)}$$

$$\frac{1}{A_{z3}} \frac{d\dot{m}_3}{dt} = -\frac{W_3}{A_{z3}} \dot{m}_3 - \frac{\Delta p_3}{(z_I - z_{I-1})} + \rho_3 g$$

$$\frac{1}{A_{z4}} \frac{d\dot{m}_4}{dt} = -\frac{W_4}{A_{z4}} \dot{m}_4 - \frac{\Delta p_4}{(z_{I+1} - z_I)} - \rho_4 g$$

$$\frac{1}{A_{\theta 5}} \frac{d\dot{m}_5}{dt} = -\frac{W_5}{A_{\theta 5}} \dot{m}_5 - \frac{1}{r_N} \frac{\Delta p_5}{(\theta_M - \theta_{M-1})}$$

$$\frac{1}{A_{\theta 6}} \frac{d\dot{m}_6}{dt} = -\frac{W_6}{A_{\theta 6}} \dot{m}_6 - \frac{1}{r_N} \frac{\Delta p_6}{(\theta_{M+1} - \theta_M)}$$

# Temporal Discretization

---

$$\frac{(r_N - r_{N-1})}{A_{r1}} \frac{\dot{m}_1^{k+1} - \dot{m}_1^k}{\Delta t} = (1 - \Theta) \left( -\frac{(r_N - r_{N-1})}{A_{r1}} W_{r1} \dot{m}_1 - \Delta p_{r1} \right)^k + \Theta \left( -\frac{(r_N - r_{N-1})}{A_{r1}} W_{r1} \dot{m}_1 - \Delta p_{r1} \right)^{k+1}$$

$$\frac{(r_N - r_{N+1})}{A_{r2}} \frac{\dot{m}_2^{k+1} - \dot{m}_2^k}{\Delta t} = (1 - \Theta) \left( -\frac{(r_N - r_{N+1})}{A_{r2}} W_{r2} \dot{m}_2 - \Delta p_{r2} \right)^k + \Theta \left( -\frac{(r_N - r_{N+1})}{A_{r2}} W_{r2} \dot{m}_2 - \Delta p_{r2} \right)^{k+1}$$

- 
- 
-

# Cont..

If we extract the  $\dot{m}^{k+1}$  terms

$$\dot{m}_1^{k+1} = \frac{\left( \frac{1}{\Delta t} - (1 - \Theta)W_{r1}^k \right)}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)} \dot{m}_1^k - \frac{A_{r1}}{(r_N - r_{N-1})} \frac{(1 - \Theta)\Delta p_{r1}^k + \Theta\Delta p_{r1}^{k+1}}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)}$$

$$\dot{m}_2^{k+1} = \frac{\left( \frac{1}{\Delta t} - (1 - \Theta)W_{r2}^k \right)}{\left( \frac{1}{\Delta t} + \Theta W_{r2}^{k+1} \right)} \dot{m}_2^k - \frac{A_{r2}}{(r_N - r_{N+1})} \frac{(1 - \Theta)\Delta p_{r2}^k + \Theta\Delta p_{r2}^{k+1}}{\left( \frac{1}{\Delta t} + \Theta W_{r2}^{k+1} \right)}$$

- 
-

# Cont ...

---

Expansion of the  $dm/dt$  for a gas yields:

$$\frac{dm}{dt} = V \cdot \frac{\partial \rho}{\partial t}$$

$$\frac{\partial \rho}{\partial t} = \left. \frac{\partial \rho}{\partial T} \right|_{p=\text{const.}} \frac{\partial T}{\partial t} + \left. \frac{\partial \rho}{\partial p} \right|_{T=\text{const.}} \frac{\partial p}{\partial t}$$

By the use of the ideal gas law or equation of state

$$\rho = \frac{p}{RT}$$

$$\rho_{\text{He}} = \frac{48.14 \frac{p}{T}}{1.0 + 0.4446 \frac{p}{T^{1.2}}}$$

# Discrete form of the continuity

---

$$V \frac{\Delta \rho}{\Delta t} = (1-\Theta) \sum_{j=1}^6 \dot{m}_j^k + \Theta \sum_{j=1}^6 \dot{m}_j^{k+1}$$

If we insert the  $\dot{m}^{k+1}$  we derived from momentum and express the density terms considering ideal gas law or equation of state, we can come up with an expression for the pressure

# Cont...

$$\begin{aligned}
 & p_{I,N,M}^{k+1} \left\{ C'_1 + \Theta^2 \left[ \frac{A_{r1}}{(r_N - r_{N-1})} \frac{1}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)} + \dots \right] - p_{I,N-1,M}^{k+1} \Theta^2 \left[ \frac{A_{r1}}{(r_N - r_{N-1})} \frac{1}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)} \right] \right\} \\
 & - p_{I,N+1,M}^{k+1} \dots - p_{I-1,N,M}^{k+1} \dots - p_{I+1,N,M}^{k+1} \dots - p_{I,N,M-1}^{k+1} \dots - p_{I,N,M+1}^{k+1} \dots \\
 & = \Theta^2 \left[ \frac{A_{z3}}{(z_I - z_{I-1})} \frac{(\rho_3 g \Delta z_3)^{k+1}}{\left( \frac{1}{\Delta t} + \Theta W_{z3}^{k+1} \right)} - \frac{A_{z4}}{(r_{I+1} - r_I)} \frac{(\rho_4 g \Delta z_4)^{k+1}}{\left( \frac{1}{\Delta t} + \Theta W_{z4}^{k+1} \right)} \right] + \Theta \left[ \frac{\left( \frac{1}{\Delta t} - (1-\Theta) W_{r1}^k \right)}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)} m_1^k + \dots \right] \\
 & + \Theta(1-\Theta) \left[ \frac{A_{r1}}{(r_N - r_{N-1})} \frac{\Delta p_{r1}^k}{\left( \frac{1}{\Delta t} + \Theta W_{r1}^{k+1} \right)} - \dots \right] \\
 & + (1-\Theta)(m_1 + m_2 + m_3 + m_4 + m_5 + m_6)^k + p_{I,N,N}^k \cdot C'_2 + C'_3
 \end{aligned}$$

# Neutron Diffusion Equation in Discrete Form

---

$$\begin{aligned}
 & -D_{grL} S_{rL} \bar{\phi}_{grL} - D_{grR} S_{rR} \bar{\phi}_{grR} \\
 & -D_{g\theta L} S_{\theta L} \bar{\phi}_{g\theta L} - D_{g\theta R} S_{\theta R} \bar{\phi}_{g\theta R} \\
 & -D_{gzL} S_{zL} \bar{\phi}_{gzL} - D_{gzR} S_{zR} \bar{\phi}_{gzR} \\
 & + \left( \begin{array}{l} D_{grL} S_{rL} + D_{grR} S_{rR} + D_{g\theta L} S_{\theta L} \\ + D_{g\theta R} S_{\theta R} + D_{gzL} S_{zL} + D_{gzR} S_{zR} \\ + \left( \Sigma_{ag} + \sum_{g \neq g'} \Sigma_{sg'g} \right) V^l \end{array} \right) \bar{\phi}_g \\
 & = \left( \sum_{g \neq g'} \Sigma_{sgg'} + \frac{\chi_g}{k_{eff}} \sum_{g'} v \Sigma_{fg'} \right) \bar{\phi}_g V^l
 \end{aligned}$$

# Cross Section Model

---

- Native Format

$$\begin{aligned}\Sigma(\alpha, T_f, T_m, D_m, S_b) = & \Sigma^r + \alpha \Delta \Sigma^{cr} + \frac{\partial \Sigma}{\partial \sqrt{T_f}} \Delta \sqrt{T_f} + \frac{\partial \Sigma}{\partial T_m} \Delta T_m \\ & + \frac{\partial \Sigma}{\partial S_b} \Delta S_b + \frac{\partial \Sigma}{\partial D_m} \Delta D_m + \frac{\partial^2 \Sigma}{\partial D_m^2} (\Delta D_m)^2\end{aligned}$$

- 5-D Interpolation for the PBMR
  - Fuel and Moderator Temperatures
  - Fast and Thermal bucklings
  - Xenon concentration

# Anisotropic Diffusion Coefficients

---

- Treatment of the void regions in PBR
- Use of radial and axial diffusion coefficients
- Obtained from analytical optimization process
- For a reactor with a height-to-radius ratio above 1

$$D_r = 0.1R$$

$$D_z = 0.5R$$

# Linear System Solvers

---

- PARCS linear system solver
  - Preconditioned Conjugate Gradient (PCG)
  - MILU (Modified Incomplete LU) preconditioner
- Other solvers investigated from the IMSL library
  - DPCGRC: Jacobi Preconditioned Conjugate Gradient
  - DGMRES: Generalized Minimum Residual
  - DLXLG: Sparse system with Gauss Elimination
  - DLXLRG: Gauss Elimination

# PARCS/THERMIX-3D Coupling

---

- Thermix is merged into PARCS source.
- Called as a subroutine when T/H feedback is required.
- Uses same coarse mesh structure
- Mapping is performed automatically

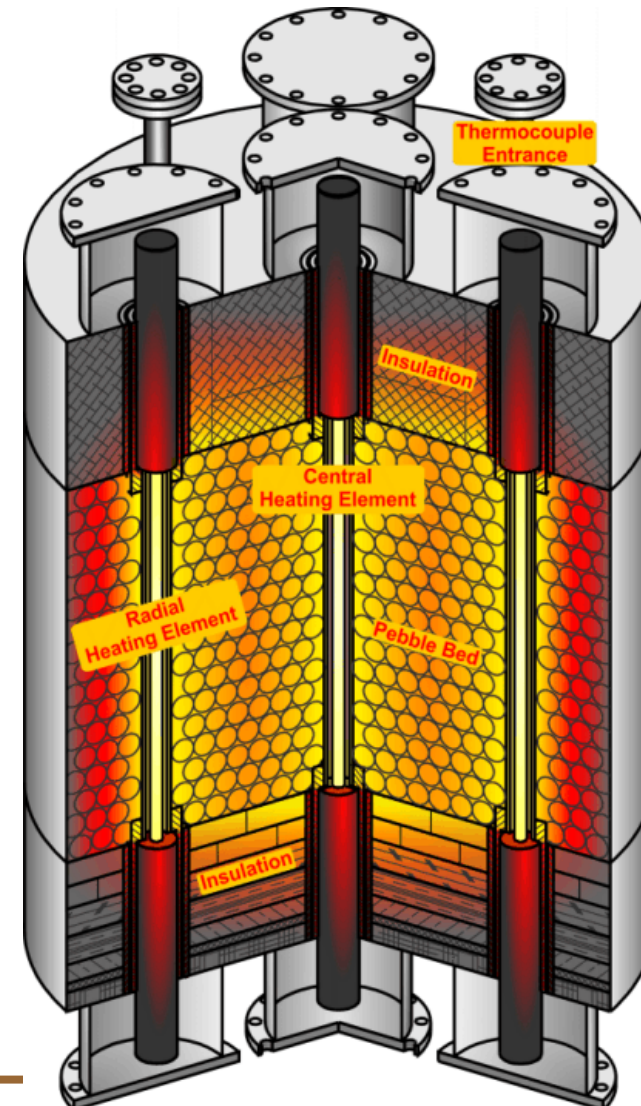
# VERIFICATION STUDIES

---

- SANA experiment
  - Standalone Thermal-Hydraulics
  
- PBMR-400 benchmark problem
  - Standalone Neutronics
  - Standalone Thermal-Hydraulics
  - Couple Neutronics/ Thermal-Hydraulics

# SANA Test Facility

- Bed of graphite pebbles in a cylindrical arrangement.
- Diameter of 1.5 m and a height of 1 m
- Approximately 9500 graphite pebbles with a diameter of 6 cm
- Heat is produced by the 4 electrical resistance heating element

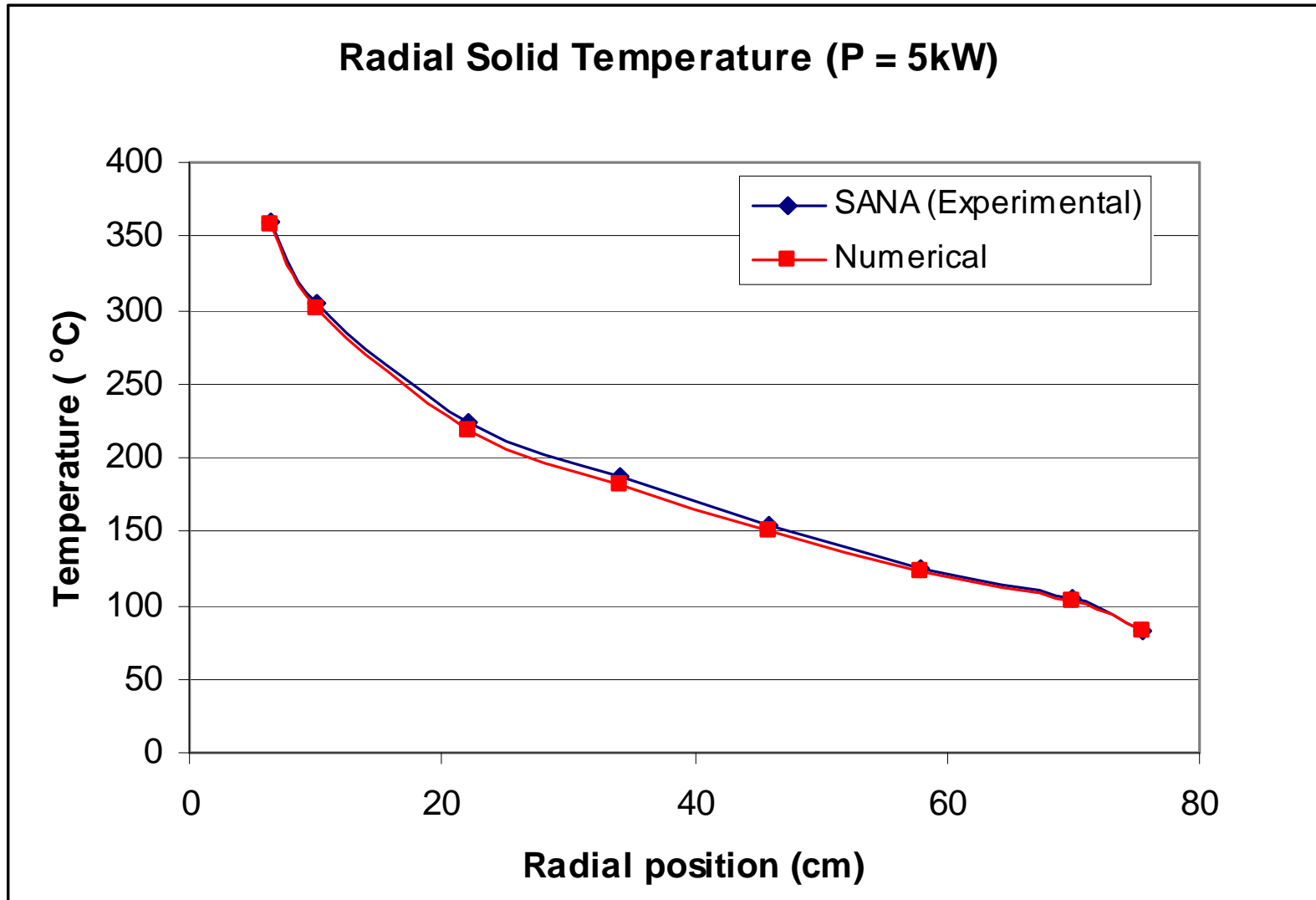


# Test-1&2

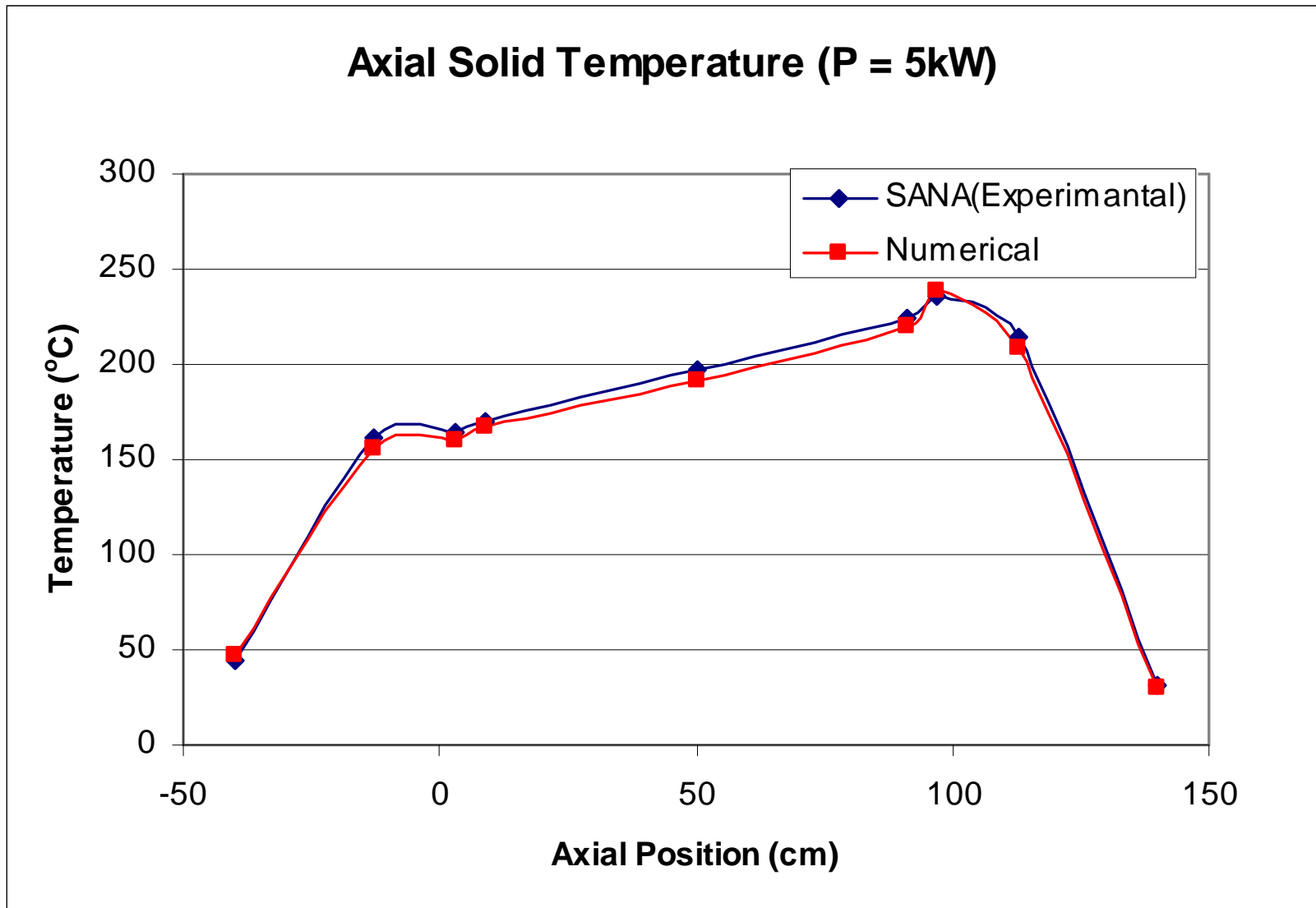
---

- Steady State
- Long heating element in the centre
- 6 cm diameter pebbles
- Cooled by helium
- **Test-1** with **5kW** power
- **Test-2** with **30kW** power

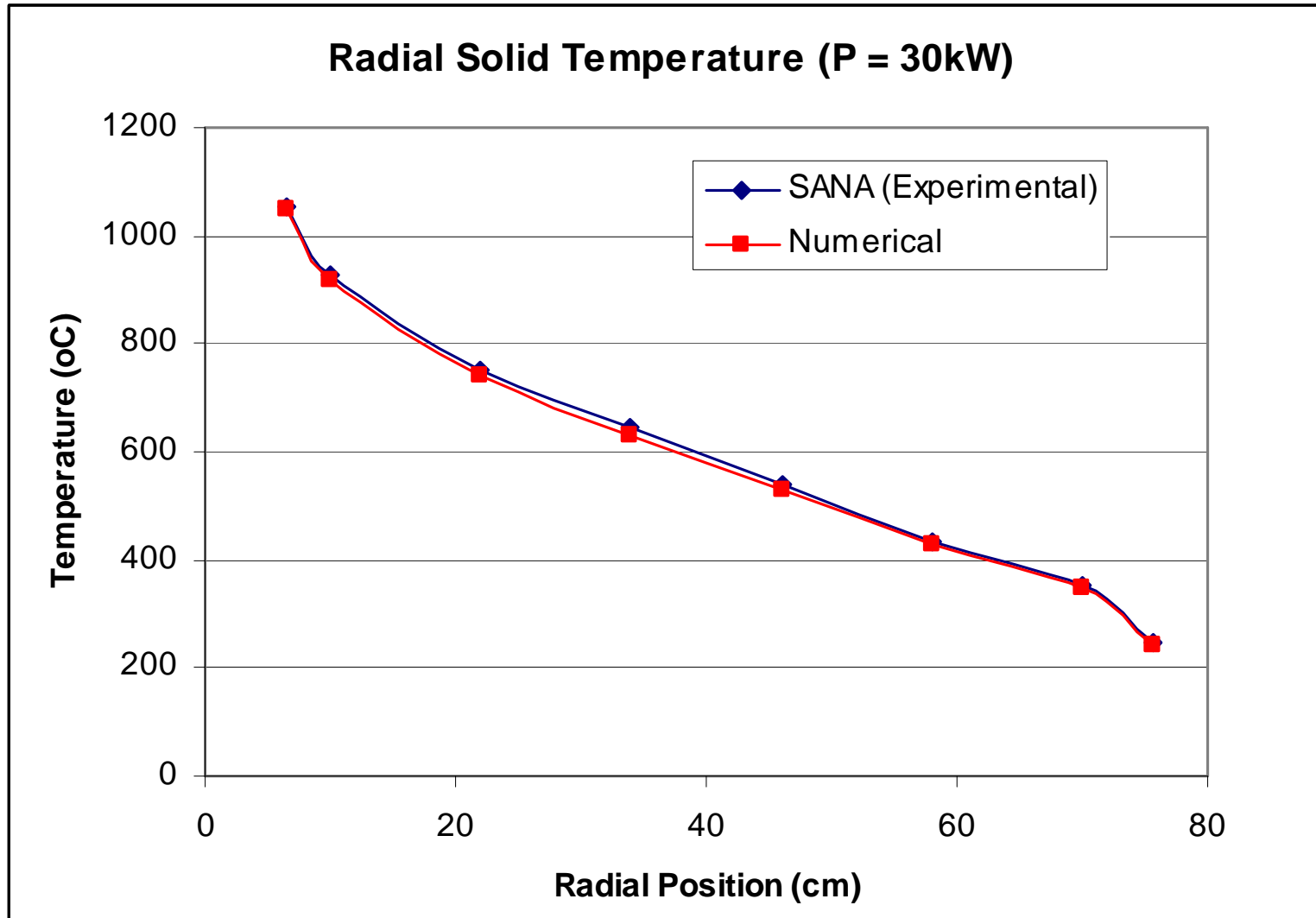
# Results of Test 1&2



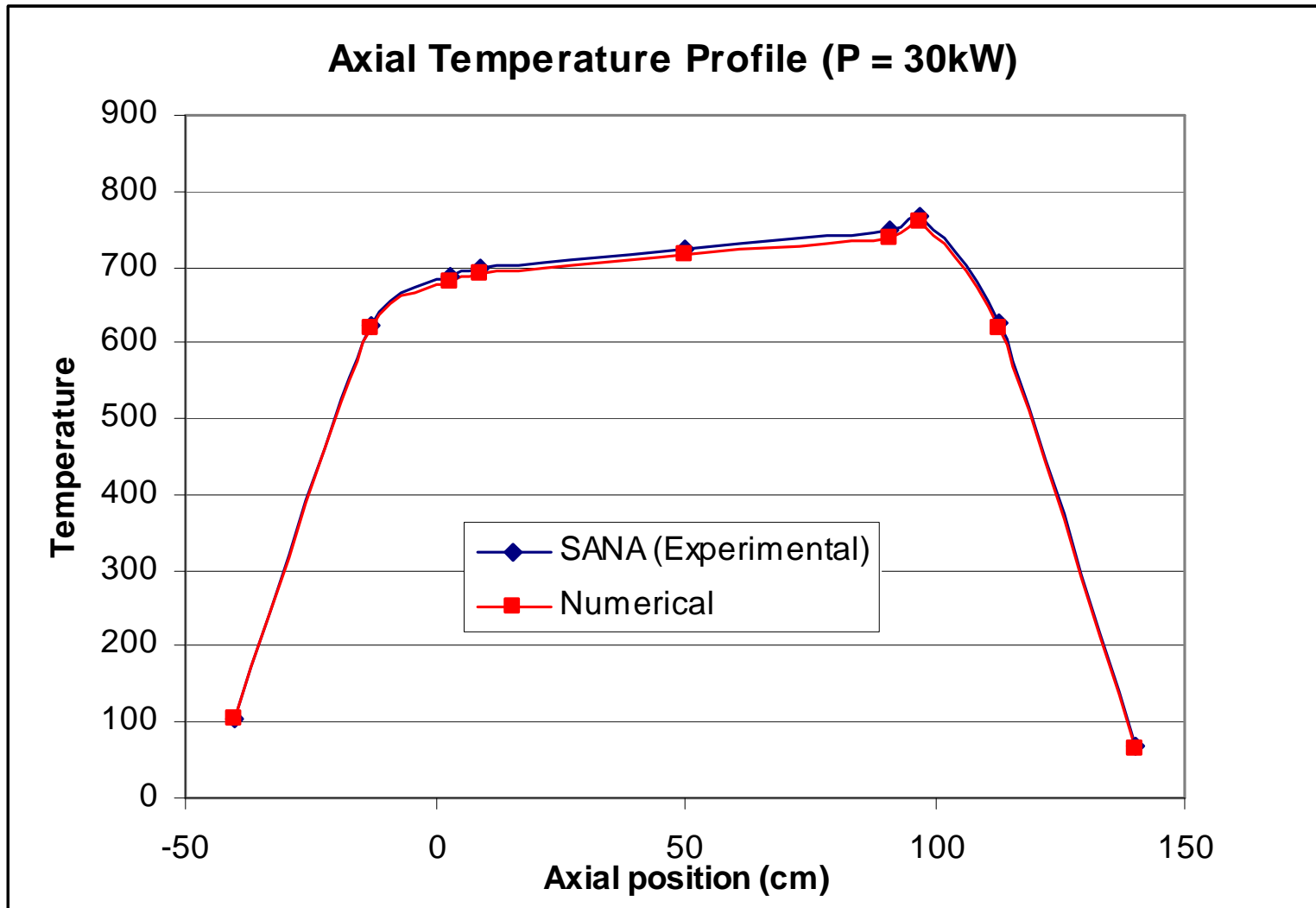
# Cont ...



# Cont ...

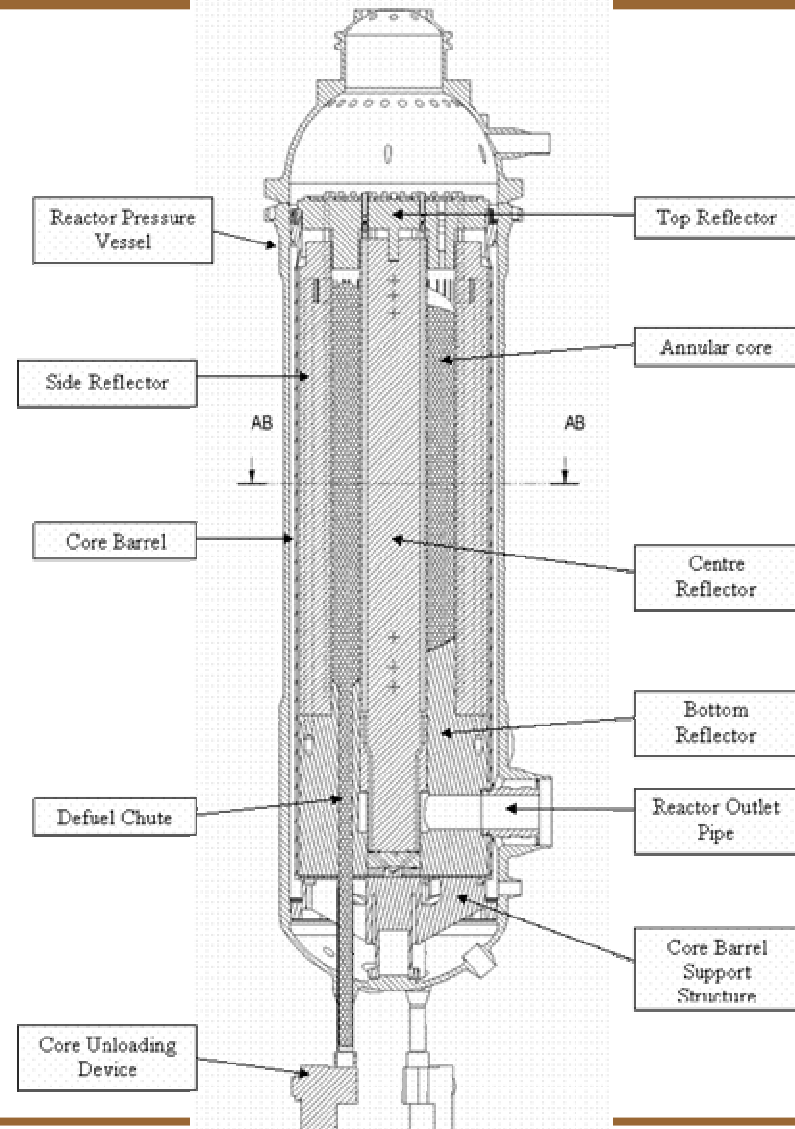


# Cont ...



# PBMR-400 Benchmark Problem

PBMR Characteristic	Value
Thermal Power	400 MW
Core configuration	Vertical with fixed centre graphite reflector
Outer diameter	3.7 m
Core Height	11 m
Reactor pressure	9MPa
Mass flow rate	192.5 kg/s
Core inlet temperature	500°C.



# Benchmark Specification

---

- 2-D (r-z) for all cases except control rod ejection (requires 3-D)
- flattened pebble bed's upper surface and bottom cones
- pebble flow is in parallel channels and at equal speed.
- Use of 5-D cross section.

# Core Layout

	0	12	41	73.0	88.58	92.06	100	117	134	151	168	182.06	204.45	211.4	225	243.0	260.0	278	287.8	302.6	310	328	462	483	
	10	31	32.6	6.96	11.5	7.95	11	11	11	11	11	1.95	11.5	6.95	13.6	18.6	11	11.4	12.5	5	11.6	18	134	11	
	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP	TP
-200	36																								
-150	50	CC	CC	CC	CC	RSS	CC	TR	TR	TR	TR	TR	SR	RCS	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
-100	50	CC	CC	CC	CC	RSS	CC	TR	TR	TR	TR	TR	SR	RCS	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
-50	50	CC	CC	CC	CC	RSS	CC	TR	TR	TR	TR	TR	SR	RCS	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
0	50	CC	CC	CC	CC	RSS	CC	V	V	V	V	V	SR	RCS	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
50	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	IP	RCS	IP	IP	IP	RC	SR	He	CB	He	RPV	AI	ROCS
100	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
150	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
200	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
250	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
300	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
350	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
400	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
450	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
500	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
550	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
600	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
650	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
700	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
750	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
800	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
850	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
900	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
950	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1000	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1050	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1100	50	CC	CC	CC	CC	RSS	CC	F	F	F	F	F	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1150	50	CC	CC	CC	CC	RSS	CC	BR	BR	BR	BR	BR	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1200	50	CC	CC	CC	CC	RSS	CC	BR	BR	BR	BR	BR	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1250	50	CC	CC	CC	CC	RSS	CC	BR	BR	BR	BR	BR	SR	RCS	SR	SR	SR	RC	SR	He	CB	He	RPV	AI	ROCS
1300	50	CC	CC	CC	CC	CC	CC	BR	BR	BR	BR	BR	SR	SR	SR	SR	SR	IP	SR	He	CB	He	RPV	AI	ROCS
1350	50	CC	CC	CC	CC	CC	CC	BR	BR	BR	BR	BR	SR	SR	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
1400	50	CC	CC	CC	CC	CC	CC	OR	OR	OR	OR	OR	SR	SR	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
1450	50	CC	CC	CC	CC	CC	CC	BR	BR	BR	BR	BR	SR	SR	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
1500	50	CC	CC	CC	CC	CC	CC	BR	BR	BR	BR	BR	SR	SR	SR	SR	SR	SR	SR	He	CB	He	RPV	AI	ROCS
1525	35	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP	BP



REACTOR CORE CONTAINING THE FUEL  
 HELIUM GAP BETWEEN FUEL AND TOP REFLECTOR: VOID  
 CENTRAL REFLECTOR: GRAPHITE  
 RISER CHANNEL IN SIDE REFLECTOR: GRAPHITE  
 OUTLET PLENUM BOTTOM: GRAPHITE  
 STAGNANT HELIUM



TOP REFLECTOR: GRAPHITE  
 BOTTOM REFLECTOR: GRAPHITE  
 SIDE REFLECTOR: GRAPHITE  
 TOP PLATE: IRON: ADIABATIC BOUNDARY  
 BOTTOM PLATE: IRON: ADIABATIC BOUNDARY  
 CORE BARREL: IRON



REACTOR CONTROL SYSTEM CHANNEL: GRAPHITE / GREY CURTAIN AREA  
 RESERVE SHUTDOWN SYSTEM CHANNEL: GRAPHITE / GREY CURTAIN AREA  
 INLET PLENUM TOP / BOTTOM: GRAPHITE  
 REACTOR PRESSURE VESSEL: IRON  
 STAGNANT AIR  
 REACTOR CAVITY COOLING SYSTEM: 2DC TH BOUNDARY  
 NEUTRONIC BOUNDARY CONDITION

# Cases Analyzed

---

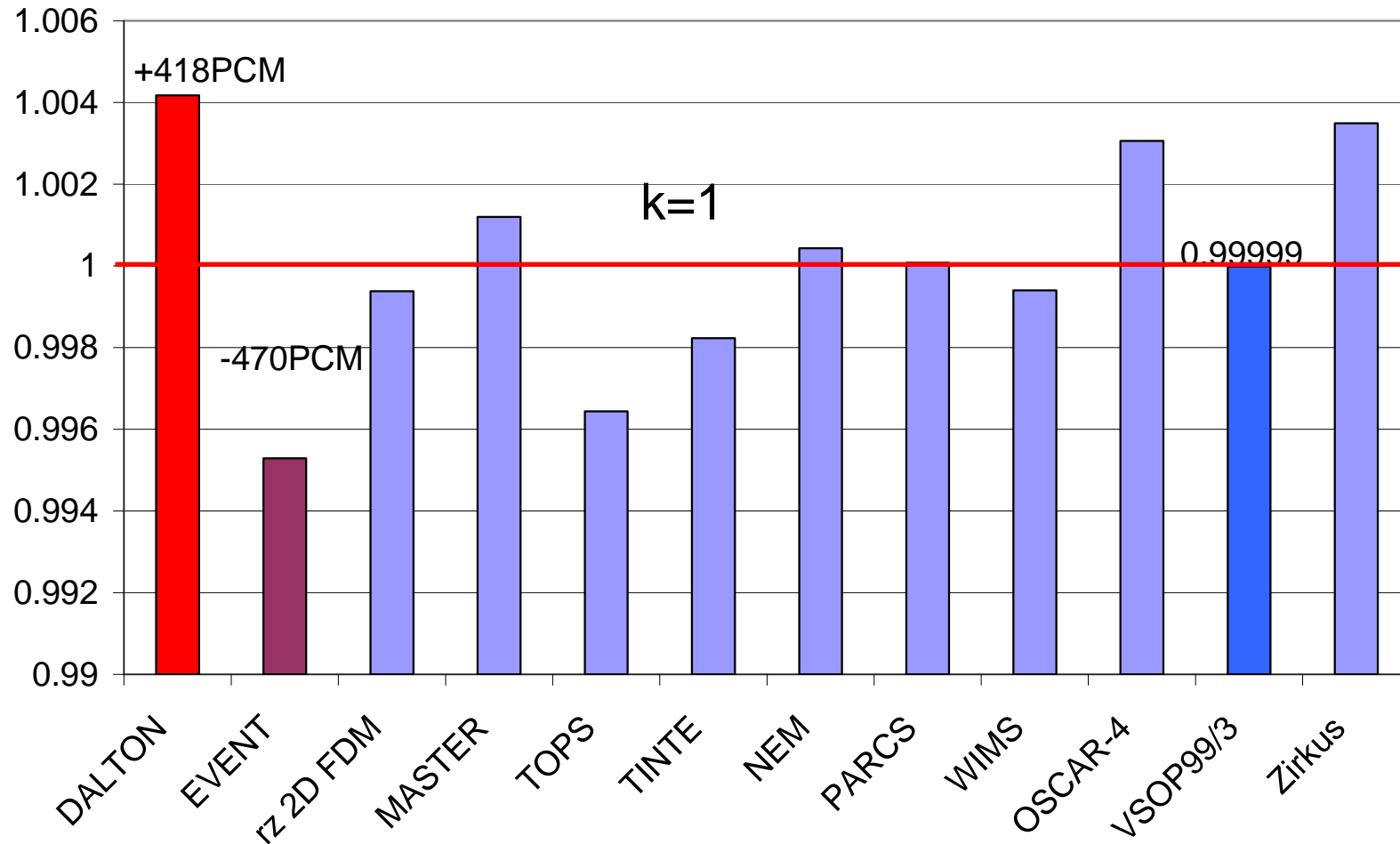
- Steady-State cases;
  - **Case S-1:** Neutronics Solution with Fixed Cross Sections
  - **Case S-2:** Thermal Hydraulic solution with given power / heat sources
  - **Case S-3:** Combined neutronics thermal hydraulics calculation – starting condition for the transients
- Transient Cases;
  - **Case T-5:** Control Rod Ejection: All 24 control rods are ejected in 0.1 sec.

# PARTICIPANTS

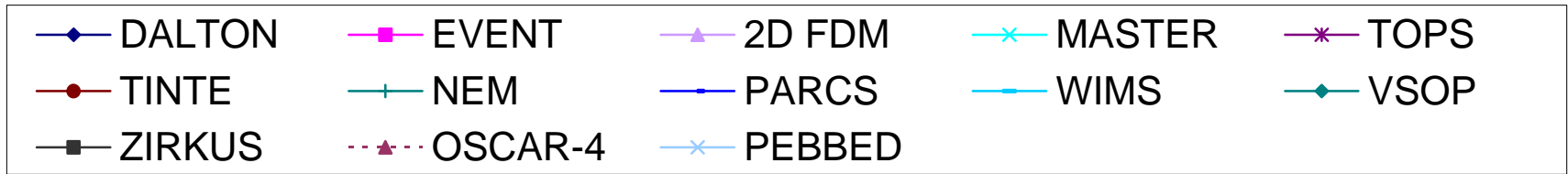
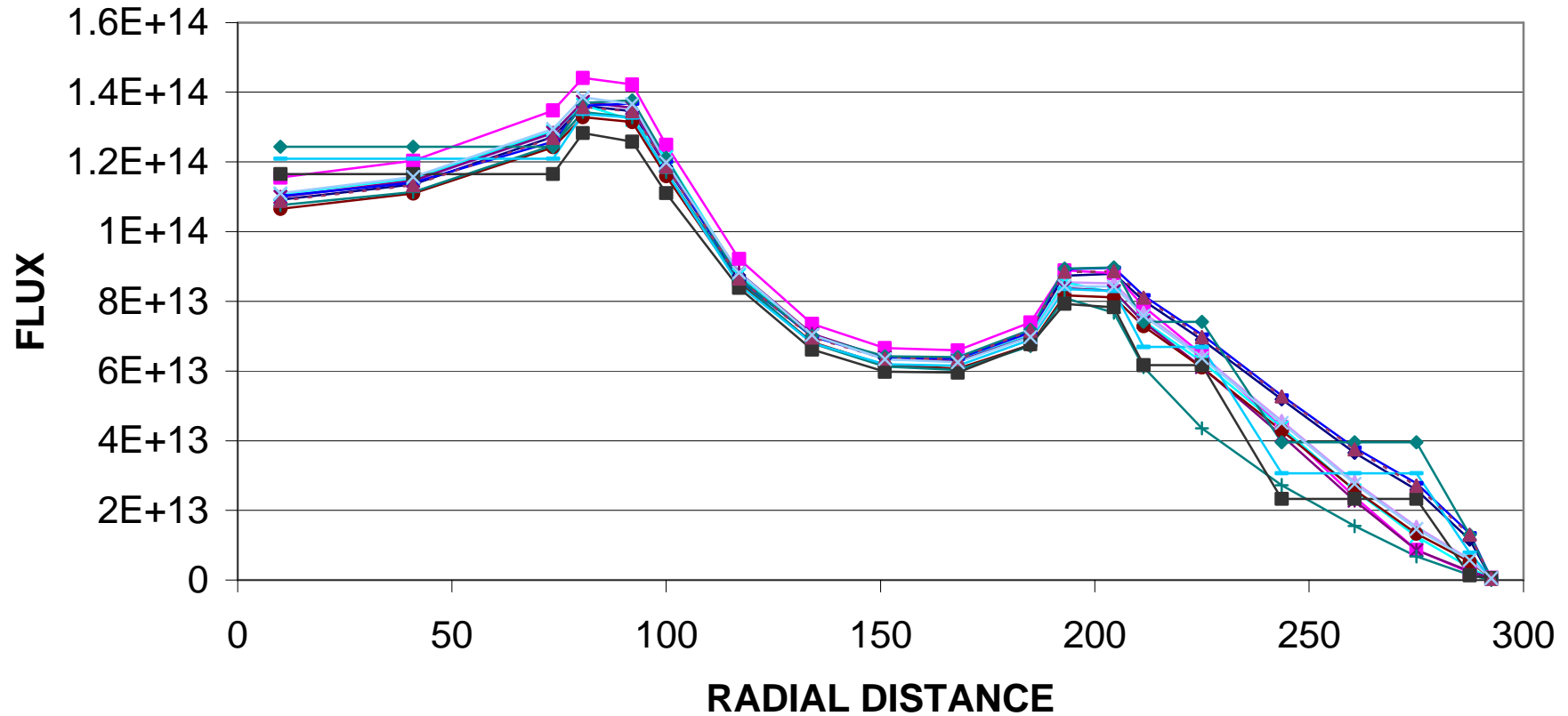
Delft-Diffusion	B.Boer	the Netherlands	3D Diffusion code (used in R-Z mode)
Delft-EVENT	B.BOER, C. DE OLIVEIRA	the Netherlands, USA	EVENT
KAERI-FDM	Hyun Chul Lee (KAERI)	KOREA	rz 2D FDM
KAERI-MASTER	Hyun Chul Lee, Jae Man Noh (KAERI)	KOREA	MASTER
KAIST	Nam Zin Cho (KAIST)	Republic of Korea	TOPS
PBMR-TINTE	PBMR	RSA	TINTE
PSU-INL	The Pennsylvania State University & Idaho National Laboratory	U.S.A	NEM
Purdue University	Purdue University	USA	PARCS & DIREKT
Serco Assurance	Serco Assurance	UK	WIMS
NECSA	NECSA	South Africa	OSCAR-4
Serco Assurance	Serco Assurance	UK	WIMS
PBMR-VSOP	PBMR	South Africa	VSOP99/3

# Case S-1 Results

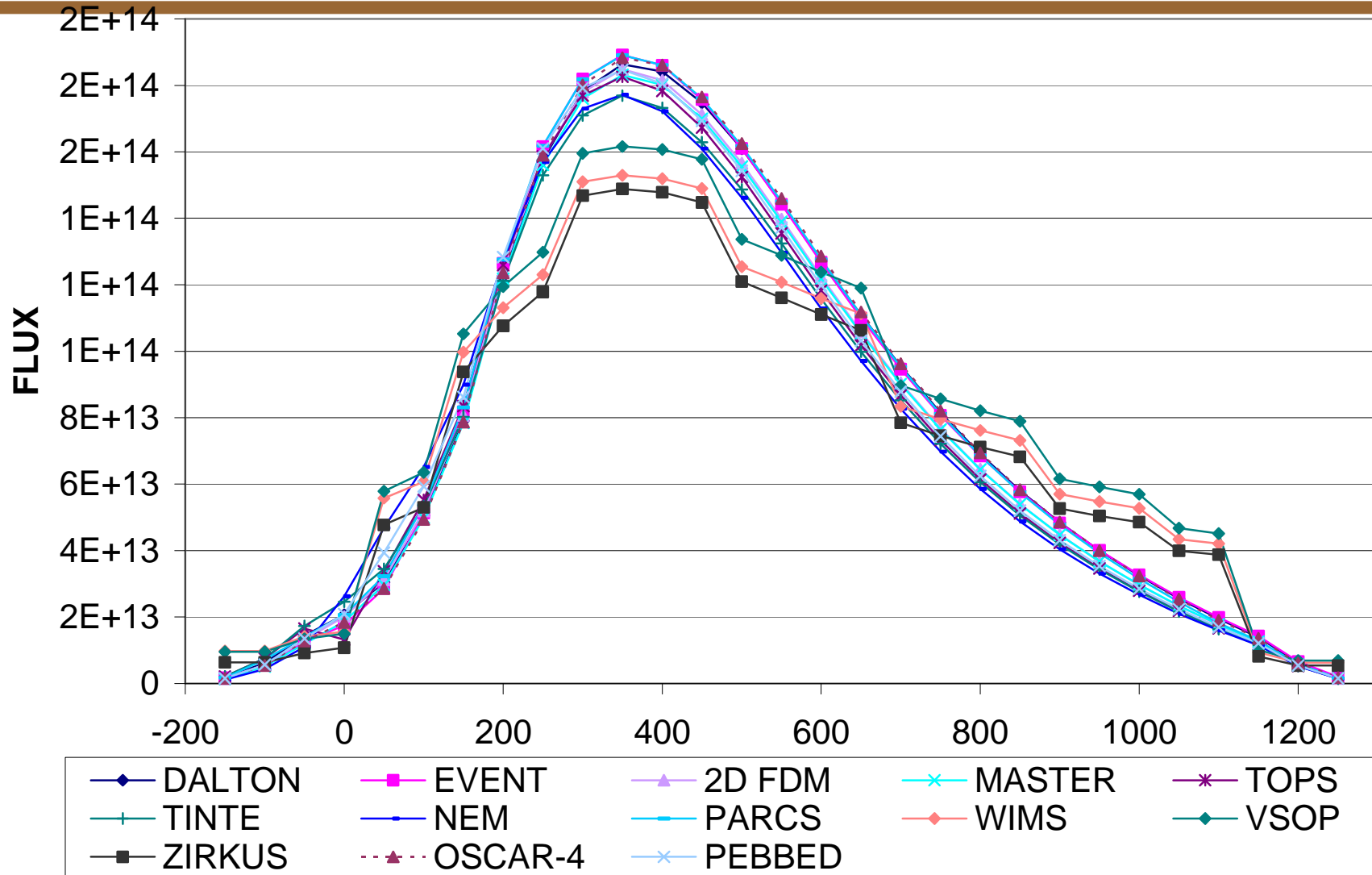
## K-EFFECTIVE



# RADIAL THERMAL FLUX



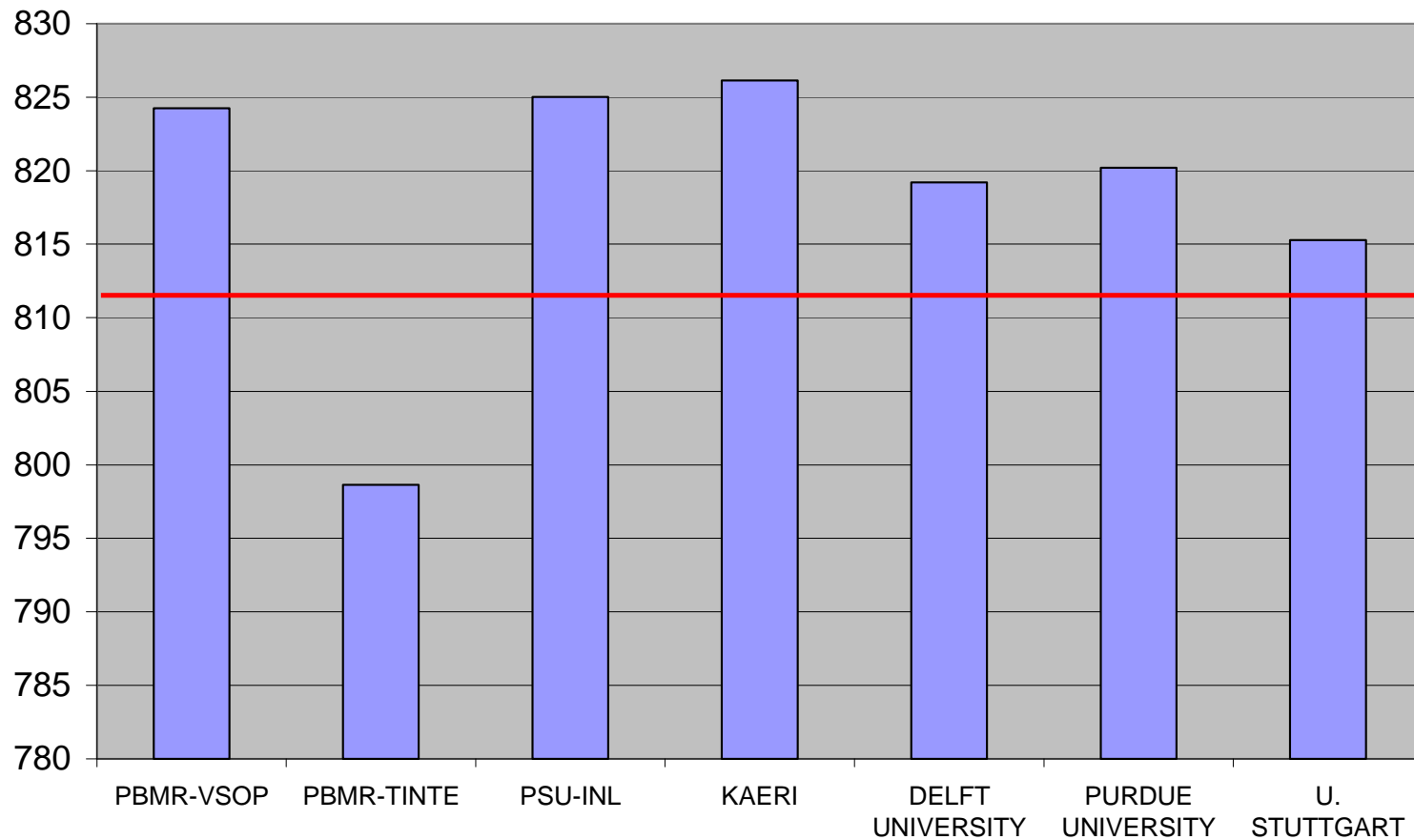
# AXIAL THERMAL FLUX



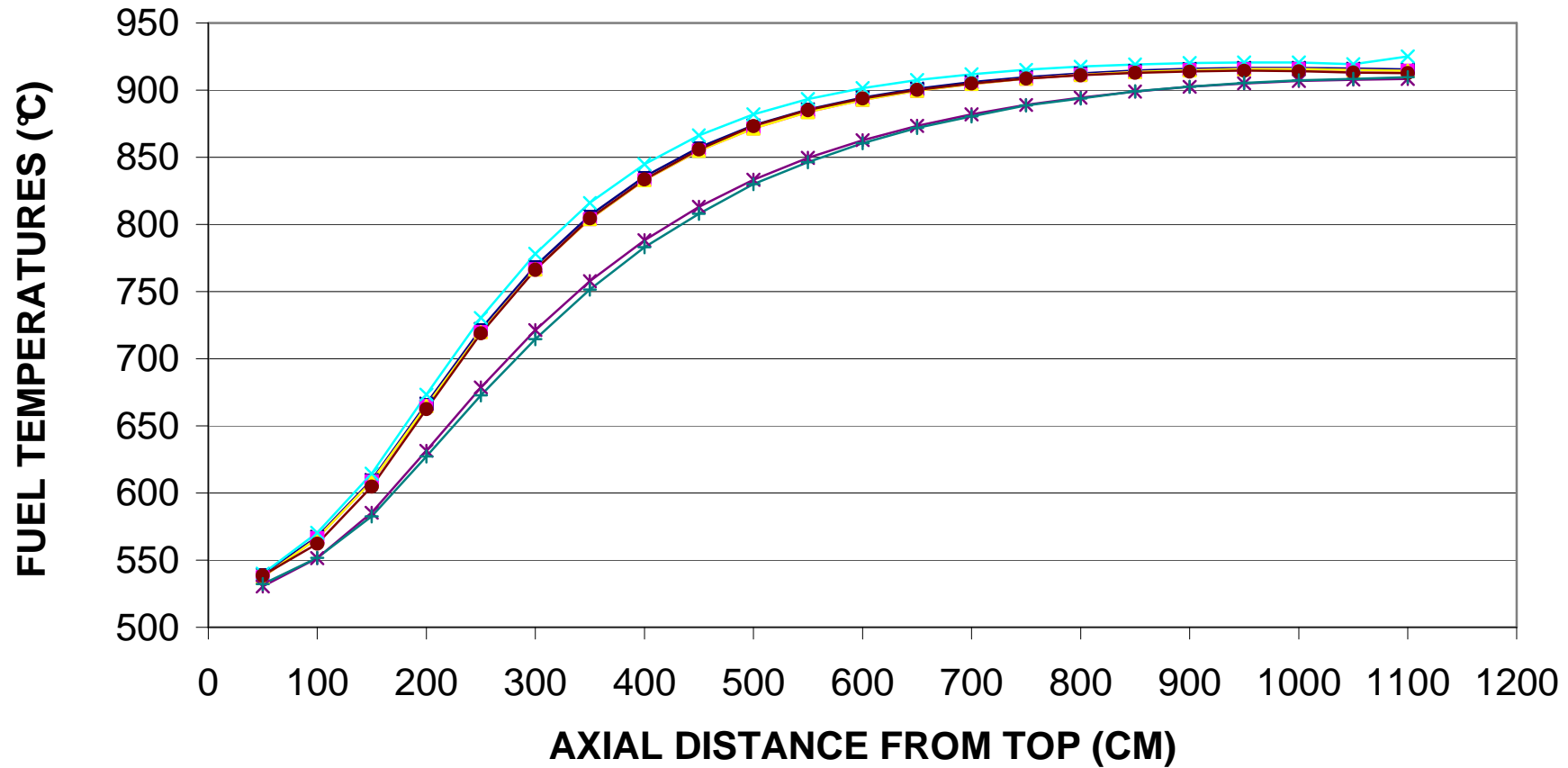
# Case S-2 Results

---

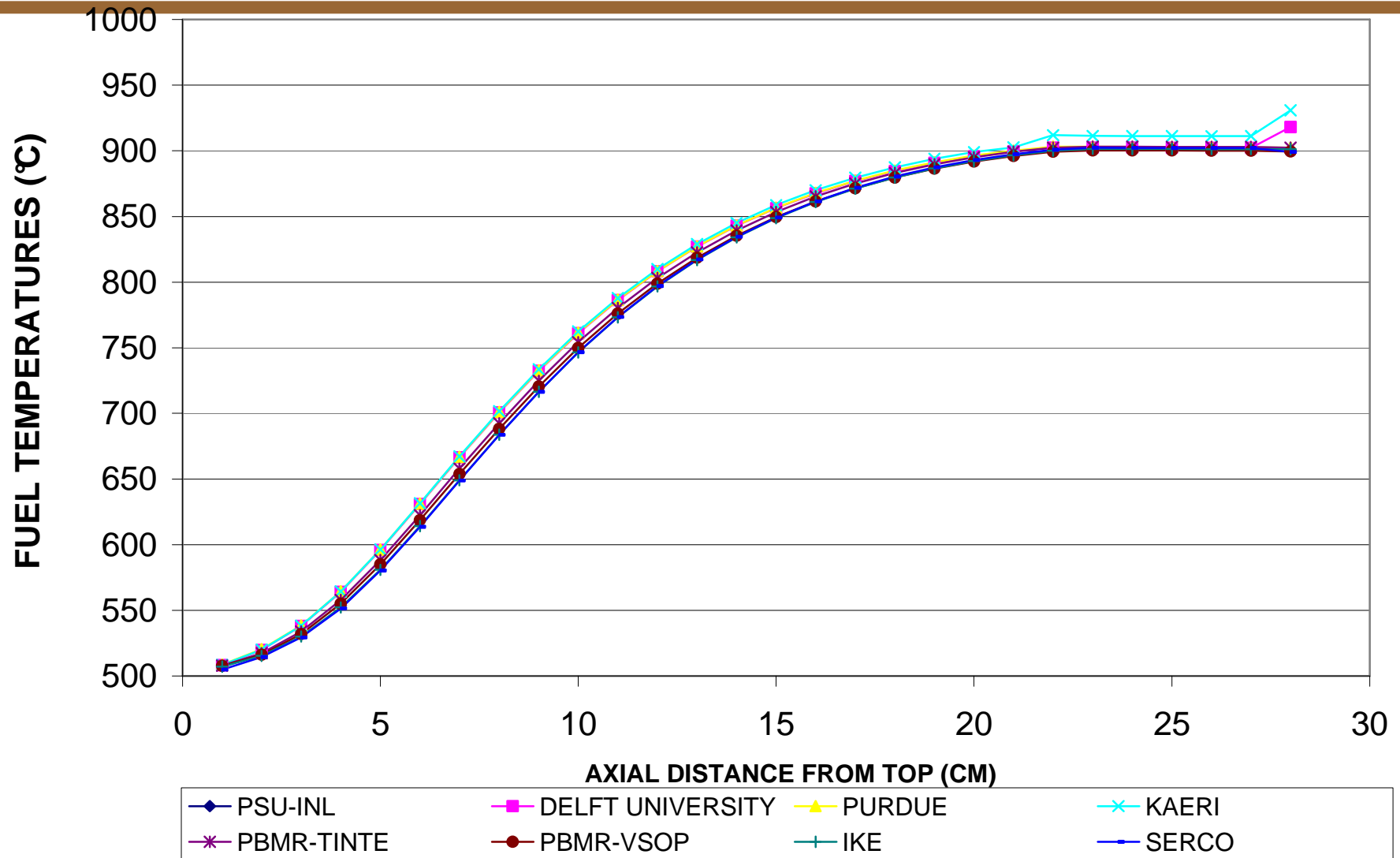
AVERAGE FUEL TEMPERATURE (°C)



## AVERAGE AXIAL FUEL TEMPERATURE PROFILE



### AVERAGE AXIAL COOLANT TEMPERATURE PROFILE

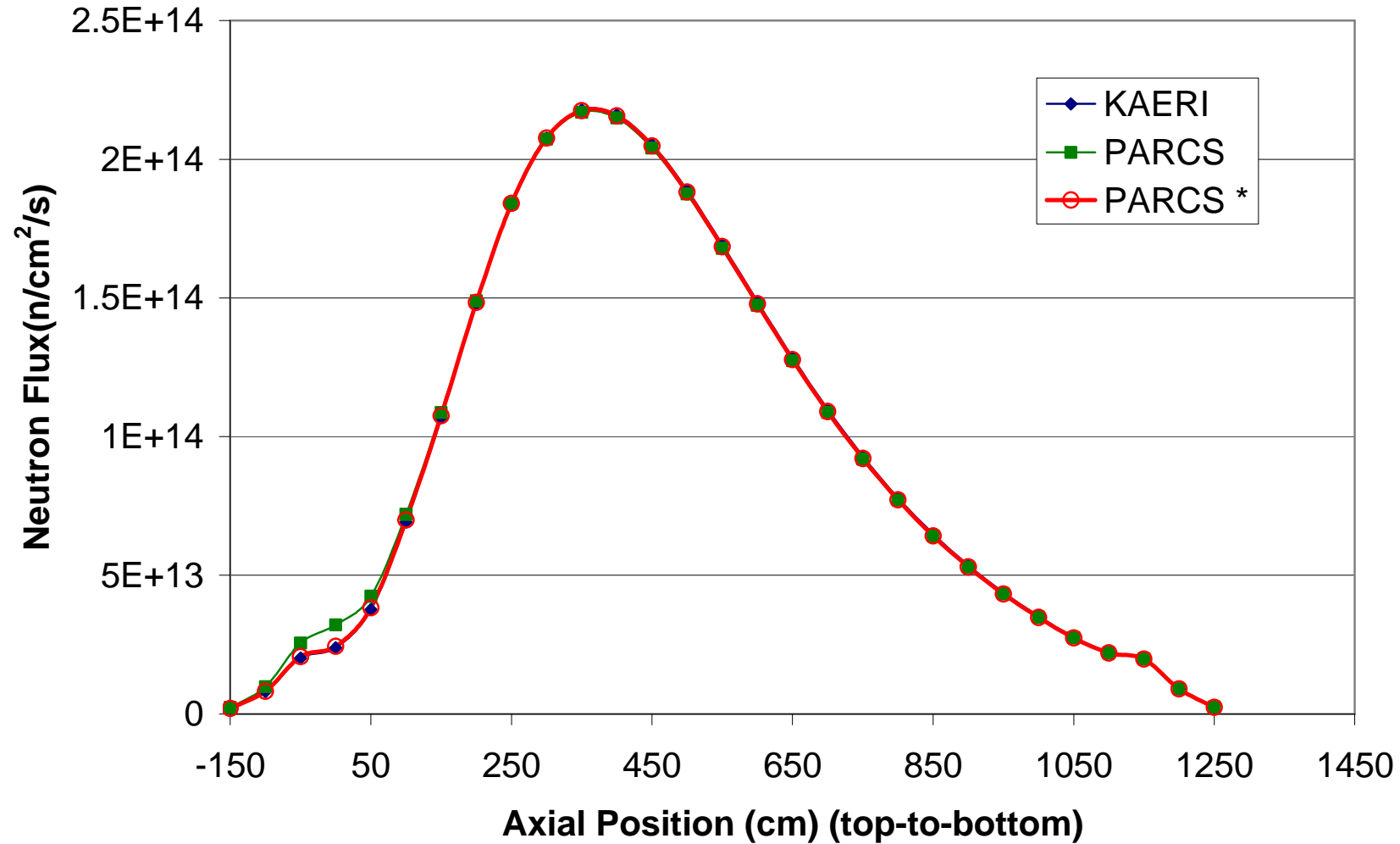


# Case S-3 Results

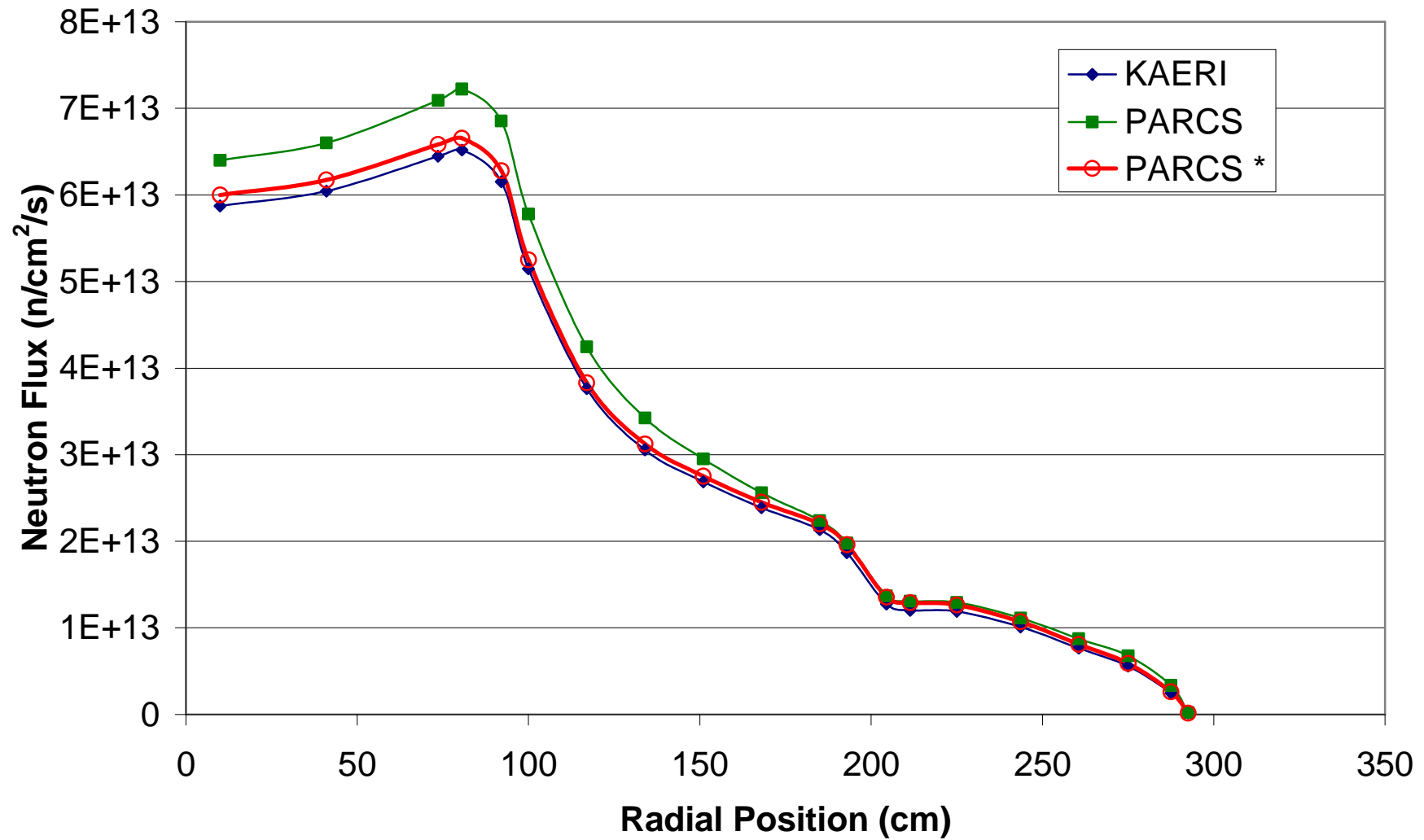
---

<b>CODE</b>	<b>keff</b>
CAPP/MARS	0.99270
PARCS	0.99283
PARCS *	0.99282
	<b>keff (at zero power)</b>
PARCS *	1.04099
KAERI	1.04090
<i>* Calculation with single diffusion coefficient</i>	

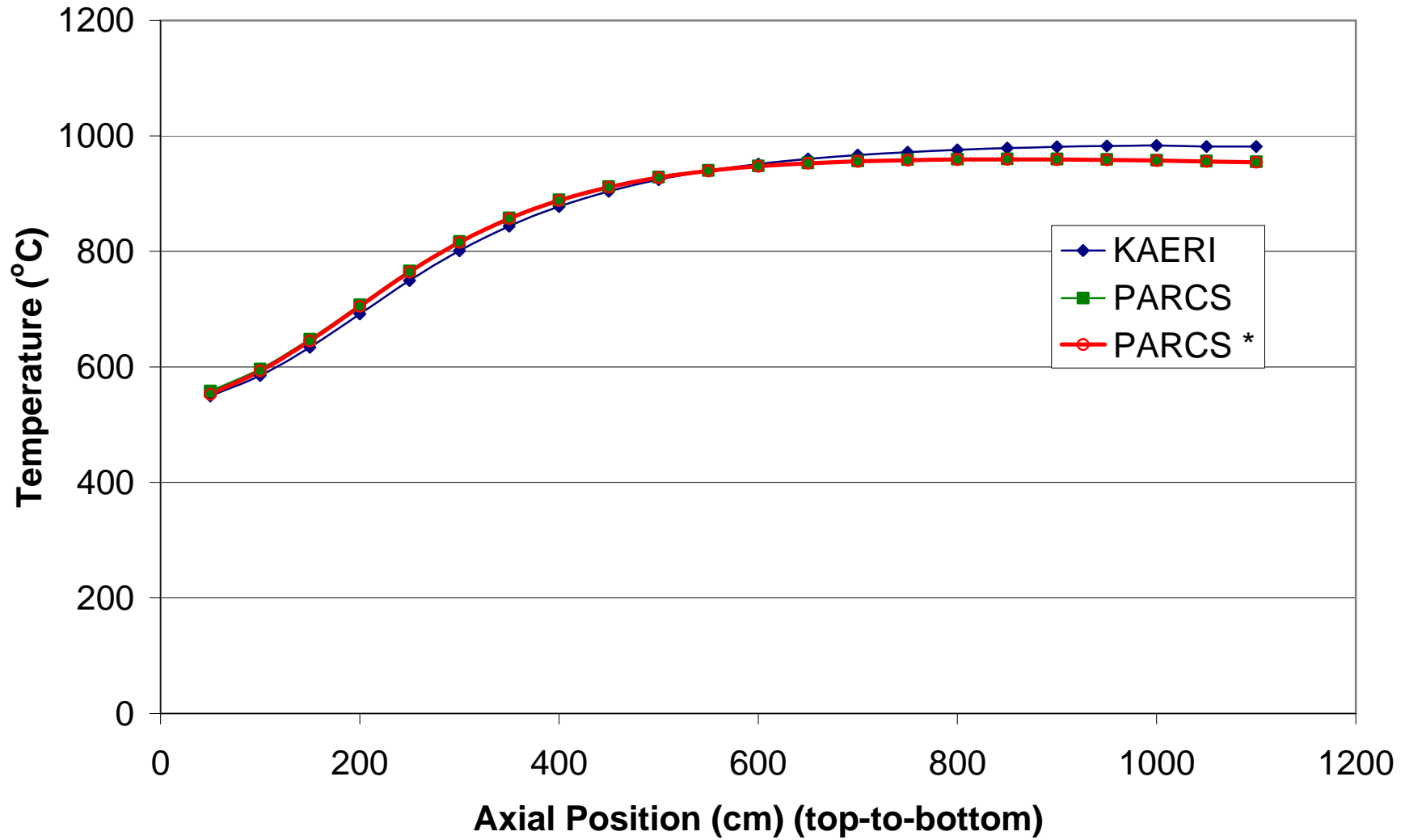
## Axial Thermal Flux



## Radial Thermal Flux (Top plane)

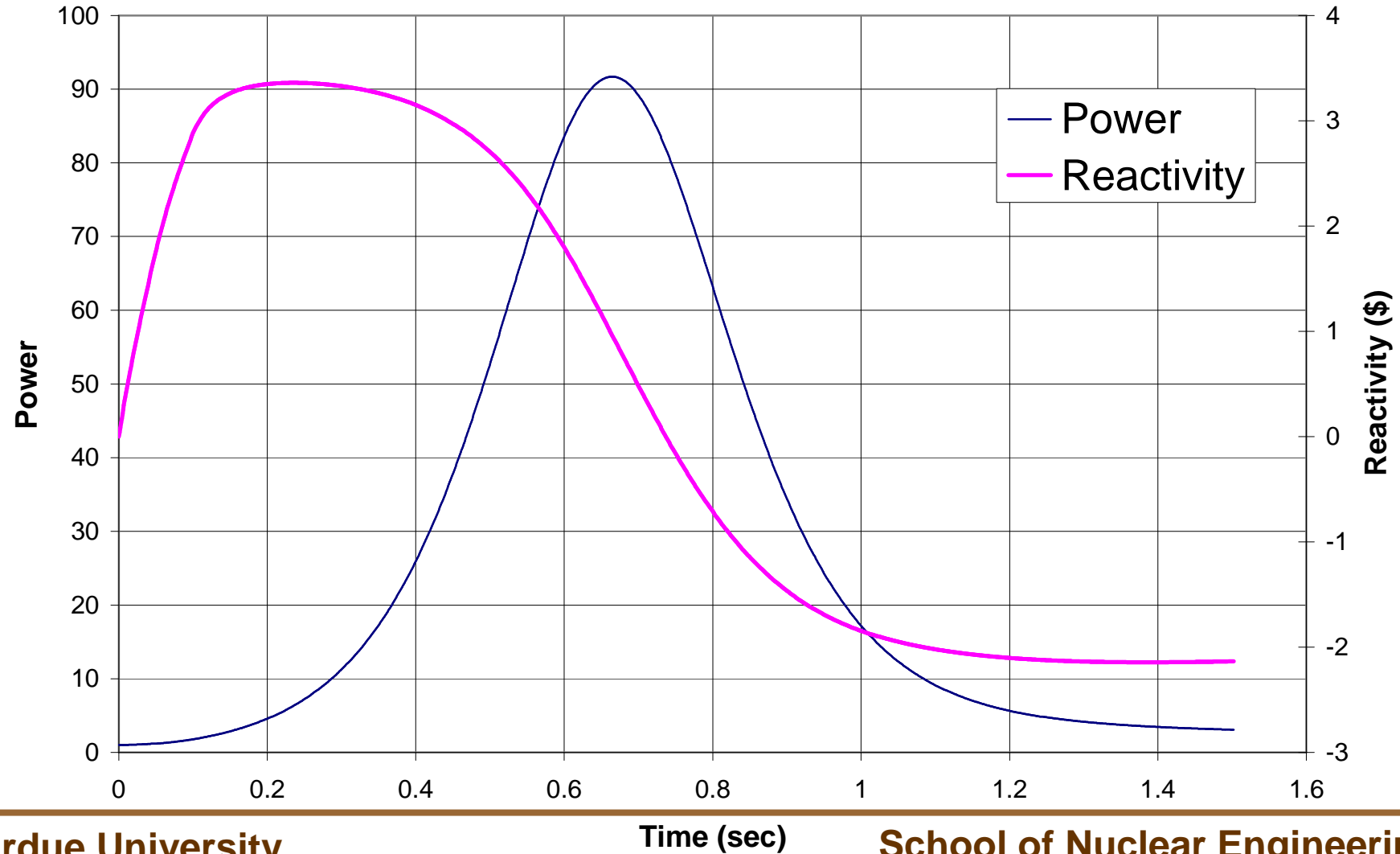


# Doppler Temperature

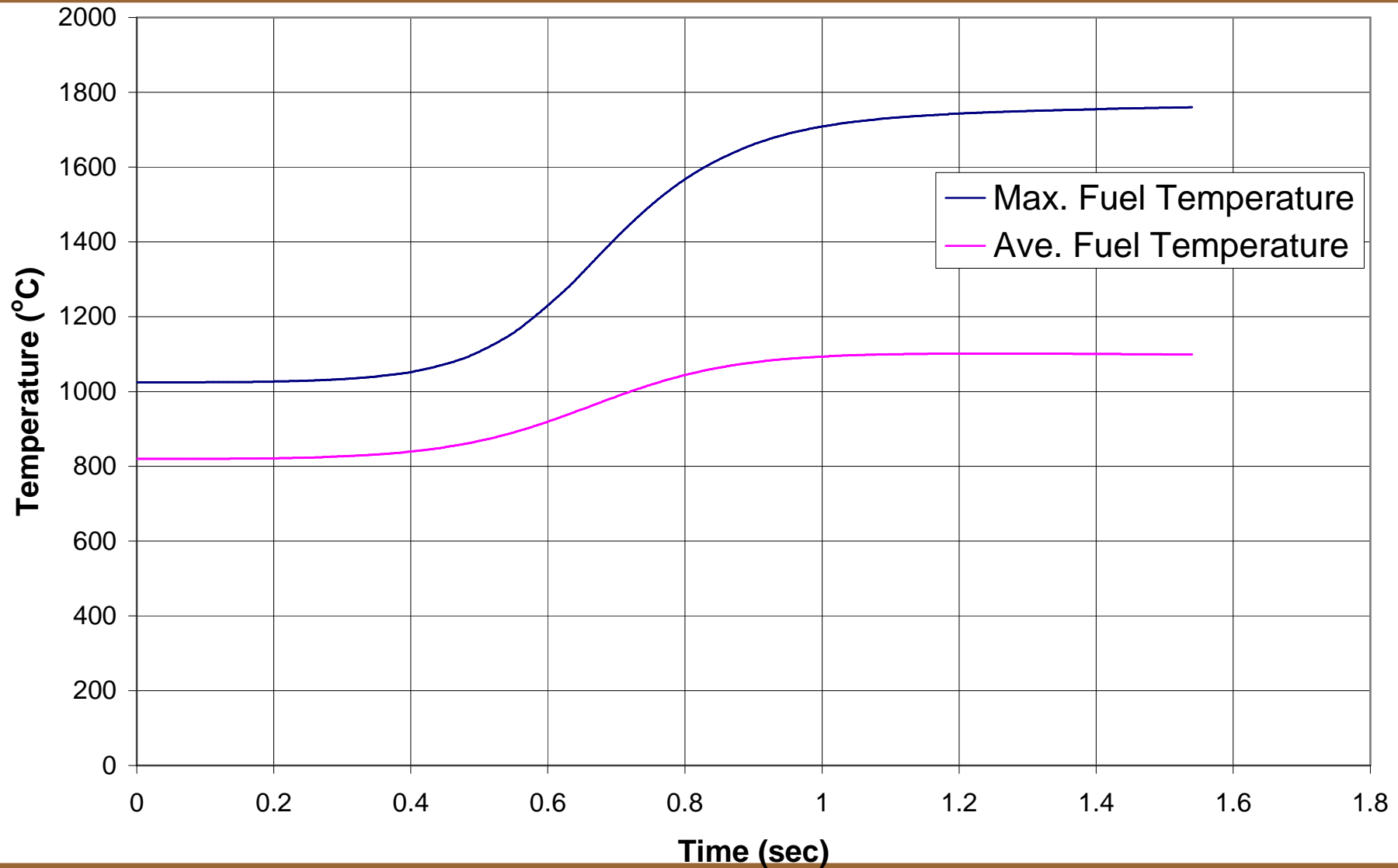


# CASE T-5 Results

## Power-Reactivity



# Fuel Temperatures



# Summary And Future Work

---

- A 3-D thermal hydraulic solver for PBRs is developed.
- A 3-D neutronics solver is developed by utilizing finite difference neutron diffusion equation.
- Verification of the standalone codes by simulating several experiments and benchmark problems has also been performed.
- Further analysis and validation is being performed for the transient conditions using the OECD/NEA PBMR-400 Benchmark